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## THE PRESSURE-VOLUME-TEMPERATURE RELATION FOR GASEOUS ETHYL ETHER. II

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In a previous paper, ${ }^{1}$ the author presented a set of measurements of pressures, volumes and temperatures for gaseous ethyl ether in which the experimental details were so arranged that the pressures were measured for the same series of specific volumes at each temperature, thus presenting data for isometrics as well as isothermals. It was pointed out that the constant-volume lines for the large specific volumes were practically straight, but as the specific volume was decreased the isometrics showed increasing curvature, which can be seen from an examination of Table I.

The data above 10 cc . per gram were used in the earlier paper for a study of the accuracy with which the Keyes equation of state reproduced the observed pressures. This equation

$$
\begin{equation*}
p=\frac{R T}{v-\delta}-\frac{A}{(v+l)^{2}}, \quad \delta=\beta e^{-\alpha / v} \tag{1}
\end{equation*}
$$

was deduced for the case of a fluid of non-varying molecular species, ${ }^{2}$ and since the degree of curvature of the isometrics was assumed by Keyes to be a measure of the association (or aggregation) effect, the equation should reproduce the measured pressures only in the region of straight isometrics. Above 15 cc . per gram the deviation between observed pressures and those calculated by Equation 1 was not over 0.05 atmosphere; for 12 cc . per gram the error was about 0.3 atmosphere, and for 10 cc . per gram, about 1.6 atmospheres.

In order to represent the pressures in the region in which the isometrics are curved it is necessary to introduce another temperature function into

[^0]Equation 1. This function must be so chosen that it straightens out the isometrics at the higher densities, without introducing any curvature into those isometrics which are already substantially linear. From an empirical standpoint this function could be introduced into either term of Equation 1 by multiplying any or all of the principal constants $R, A$ and $\beta$ by functions of the temperature and of the volume. It was shown in the previous paper that these three constants affect the calculated pressure decreasingly in the order named. Since $R$ influences the pressure to the greatest extent, the effect of multiplying $R$ by a function of $t$ and $v$ would affect the calculated pressure most directly.
Both Boltzmann ${ }^{3}$ and Jeans ${ }^{4}$ have suggested that the deviation of actual gases from the perfect gas law may be due to aggregation of the molecules, and have introduced into $R$ that function of $v$ and $t$ which is obtained from kinetic theory considerations. The results expressed qualitatively the behavior of nitrogen dioxide, but the agreement is by no means quantitative. This is probably due to the fact that the perfect gas law is too simple an equation to use as a starting point for the addition of the idea of association, as was of course recognized by these writers.
The Keyes equation has been shown to represent the observed data quite well at not too great densities, and hence the use of this equation as a basis for applying the association principle should lead to much better chances of success. It is probable that under this assumption $R, A$ and $\beta$ would all be multiplied by functions of $t$ and $v$, as well as the less important constants $\alpha$ and $l$. However, the introduction of a function of $v$ and $t$ into any of these three principal constants is approximately equivalent to its introduction into the others. Hence, for the first approximation, we can collect the whole effect and take care of it by throwing all the deviation into the gas constant $R$.
If it is assumed that the curvature of the isometrics is due to a change in the molecular species, the number of moles for a given mass of gas is changing and account must be taken of this variation of $N$, in $R$. This may be done to the first approximation by applying the mass-action equation (in its form for perfect gases) to the reaction consisting of an association of single to double molecules. Hence, the value of $R$ becomes ${ }^{5}$ $R=R_{1}(1-y / 2)$, where $(y / 2) /(1-y)^{2}=(a / v) e^{b / T}$, and $R_{1}$ is the gas constant for the unassociated molecules, $y$ the fraction associated, and $a$ and $b$ are constants usually identified with the chemical constant and the heat of association. When $y$ is small we may neglect it in comparison with 1 and write

[^1]\[

$$
\begin{equation*}
R=R_{1}\left(1-\frac{a}{v} e^{b / T}\right) \tag{2}
\end{equation*}
$$

\]

The values of $y$ calculated from the equations above have now no physical significance, since Equation 2 represents a collective effect due to the variation with the number of moles, $N$, of both $A$ and $\beta$, as well as $R$.

The equation of state then becomes

$$
\begin{gather*}
p=\frac{R T}{v-\beta e^{-\alpha / \nu}}\left(1-\frac{a}{v} e^{b / T}\right)-\frac{A}{(v+l)^{2}}  \tag{3}\\
p=\psi T(1-\gamma)-\phi \tag{4}
\end{gather*}
$$

where $\psi$ and $\phi$ are functions of volume alone and not of the temperature, and $\gamma$ is a function of both volume and temperature, that is, $(a / v) e^{b / T}$. This equation can be arranged to

$$
\begin{equation*}
p+\gamma \psi T=\psi T-\phi=p_{\text {corr }} . \tag{5}
\end{equation*}
$$

and $p+\gamma \psi T$ can be called the "corrected pressure," which should now vary linearly with the temperature at constant volume. In order to test this treatment on experimental data, it is necessary to know $\psi$ or $\left(\partial p_{\text {corr }} / \partial T\right)_{v}$ in advance in order to obtain the correction to the measured pressures. This can be obtained very accurately by two successive approximations. The value of $\partial p / \partial T$ obtained from the best straight line through the original isometric (even though it shows curvature) is used to calculate a series of provisional corrected pressures. The value of $\psi$ from these latter pressures, which now vary practically linearly with temperature, is used to calculate a new correction to be applied to the measured pressures for the final $p_{\text {corr. }}$. In the case of ether the convergence is rapid, and the greatest difference between the result of these two calculations was about 0.005 atmosphere.

In order to determine $a$ and $b$, Equation 3 can be expanded in terms of $1 / v$ after multiplying through by $v, p v=R T[1+(\beta-A / R T-$ $\left.\left.a e^{b / T}\right) 1 / v+\ldots ..\right]$ and if this expansion is compared with the isothermal equation of Kamerlingh Onnes, $p v=R T(I+B / v+\ldots .$.$) , it is evident$ that

$$
\begin{equation*}
B=\beta-A / R T-a e^{b / T} \tag{6}
\end{equation*}
$$

For each measured isotherm it is possible to determine a $B$ either analytically or by plotting $[(p v / R T)-1] v$ against $1 / v$. This plot gives a curve which tends to straighten for small values of $1 / v$, and the intercept on the $[(p v / R T)-1] v$ axis gives directly the value of $B$.
From a consideration of the $B$ values in the light of Equation 6 it is possible to obtain values for $a$ and $b$. Plotting $B$ against $1 / T$ gives a curve which approaches a straight line, at higher temperatures, where the exponential is small, but at lower temperatures shows increasing curvature.
The difference $\Delta B$ between the experimentally determined $B^{\prime}$ s and those obtained from an extension of the tangent to the high-temperature values gives a means of obtaining $a$ and $b$, for $\Delta B=a e^{b / T}$ and $\log \Delta B=$
$\log a+b / 2.3 T$. Unfortunately, $a$ and $b$ are not uniquely determined since a small variation in $\Delta B$ is due possibly to the use of judgment in drawing the tangent to the extension of the $B$ plot. However, in the case of ethyl ether, $a$ is very small so that although $a$ and $b$ are not determined absolutely by the method outlined above, the value of the whole exponential term $a e^{b / T}$ does not vary much with the different possible values of $a$ and $b$ for the temperature range of the data.
In Table I are given the values of $p_{\text {corr. }}$. compared with the pressures calculated from the best straight lines through the isometrics. $P_{\text {corr. }}$ was calculated by means of Equation 5, using the values of $\psi, a$ and $b$ obtained by the methods outlined in the preceding paragraphs. There are also included the deviations of the observed pressures from the best straight line through the original isometrics obtained from the former article. It can be seen that the observed pressures show curvature at the higher densities, while the corrected pressures are linear even down to 5 cc . per gram.

Table I
Comparison of Observed Pressures Corrected for the "Aggregation Effect" with those Calculated by Assuming the Isometric Lines to be Straight

The first line gives the observed "corrected pressures," the second those calculated from the linear equation given, and the third the observed minus the calculated pressures. The fourth line gives the deviation of the measured pressures from linearity.

$$
P_{\text {oorr. }}=P_{\text {obs. }}+T\left(\frac{\partial P_{\text {corr. }}}{\partial T}\right)_{v} \frac{0.00145}{v} e^{1596 / T}
$$

| Vol. cc./g. | Temp. <br> ${ }^{\circ} \mathrm{C} .150$ | 175 | 200 | 225 | 250 | 275 | 300 | 325 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 35 | $p=0.03685 T-4.374$ |  |  |  |  |  |  |  |
|  | 11.218 | 12.136 | 13.070 | 13.976 | 14.907 | 15.811 | 16.746 | 17.678 |
|  | 11.218 | 12.140 | 13.061 | 13.982 | 14.903 | 15.825 | 16.746 | 17.667 |
|  | 0.000 | $-0.004$ | 0.009 | $-0.006$ | 0.004 | $-0.014$ | 0.000 | 0.011 |
|  | . 003 | . 000 | . 013 | - . 004 | . 005 | - . 014 | . 002 | . 006 |

30
$\left.\begin{array}{rrrrrrrr}12.706 & 13.790 & 14.876 & 15.992 & 17.099 & 18.186 & 19.296 & 20.412 \\ 12.695 & 12.795 & 14.895 & 15.995 & 17.095 & 18.195 & 19.295 & 20.395 \\ 0.011 & -0.005 & -0.019 & -0.003 & 0.004 & -0.009 & 0.001 & 0.017 \\ .015 & .000- & .013 & .002 & .008 & - & .007 & .000\end{array}\right] .014$

25
$\left.\begin{array}{rrrrrrrr}14.537 & 15.909 & 17.273 & 18.643 & 19.993 & 21.354 & 22.737 & 24.077 \\ 14.551 & 15.913 & 17.274 & 18.635 & 19.996 & 21.358 & 22.719 & 24.080 \\ -0.014 & -0.004 & -0.001 & 0.008 & -0.003 & -0.004 & 0.018 & -0.003 \\ - & .014- & .001 & .002 & .010- & .003- & .006 & .013\end{array}\right) .012$

| $\begin{aligned} & \text { Vol,', } \\ & \text { cc./g. } \end{aligned}$ | Table I (Concluded) |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $\overbrace{\text { Temp. }}^{\text {Te. }}$ | 175 | 200 | 225 | 250 | 275 | 300 | 325 |
| 15 |  | $p=0.10103 T-22.629$ |  |  |  |  |  |  |
|  |  | 22.646 | 25.171 | 27.698 | 30.228 | 32.737 | 35.284 | 37.797 |
|  |  | 22.646 | 25.171 | 27.697 | 30.223 | 32.749 | 35.274 | 37.800 |
|  |  | 0.000 | 0.000 | 0.001 | 0.005 | $-0.012$ | 0.010 | $-0.003$ |
|  |  | - . 009 | - . 001 | . 005 | . 010 | - . 007 | . 012 | - . 005 |
| 12.5 | $p=0.12671 T-31.726$ |  |  |  |  |  |  |  |
|  |  | 25.057 | 28.226 | 31.394 | 34.562 | 37.734 | 40.891 | 44.057 |
|  |  | 25.057 | 28.224 | 31.392 | 34.560 | 37.728 | 40.895 | 44.063 |
|  |  | 0.000 | 0.002 | 0.002 | 0.002 | 0.006 | - 0.004 | - 0.006 |
|  |  | - . 019 | - . 003 | . 005 | . 009 | . 012 | - . 001 | - . 009 |
| 10 | $p=0.16733 T-47.245$ |  |  |  |  |  |  |  |
|  |  |  | 31.913 | 36.105 | 40.296 | 44.482 | 48.655 | 52.847 |
|  |  |  | 31.924 | 36.107 | 40.290 | 44.474 | 48.657 | 52.840 |
|  |  |  | - 0.011 | - 0.002 | 0.006 | 0.008 | - 0.002 | 0.007 |
|  |  |  | - . 010 | . 006 | . 013 | . 011 | - . 010 | - . 015 |
| 7.5 | $p=0.24181 T-78.257$ |  |  |  |  |  |  |  |
|  |  |  | 36.146 | 42.199 | 48.246 | 54.276 | 60.341 | 66.376 |
|  |  |  | 36.151 | 42.196 | 48.241 | 54.286 | 60.332 | 66.377 |
|  |  |  | - 0.005 | 0.003 | 0.005 | $-0.010$ | 0.009 | - 0.001 |
|  |  |  | - . 022 | . 009 | . 019 | . 001 | . 010 | - . 018 |
| 5 | $p=0.40638$ T - 151.876 |  |  |  |  |  |  |  |
|  |  |  | 40.399 | 50.551 | 60.679 | 70.904 | 81.028 | 91.197 |
|  |  |  | 40.395 | 50.554 | 60.714 | 70.873 | 81.033 | 91.192 |
|  |  |  | 0.004 | $-0.003$ | - 0.035 | 0.031 | $-0.005$ | 0.005 |
|  |  |  | - . 025 | . 020 | . 005 | . 059 | - . 009 | - . 050 |
|  | $T=t^{\circ}+273.13$ |  |  |  |  |  |  |  |

The values of $\psi$ and $\phi$ of Equation 5 for each volume can be used to study the correctness of the volume function chosen, since the corrected pressures now vary linearly with the temperature, and hence $\psi$ and $\phi$ are uniquely determined. ${ }^{6}$ If in some special case it should happen that the functions suggested by Keyes do not fit, then other functions may be tried, but $\psi$ and $\phi$ are now volume functions only, since all the temperature curvature has been removed by the exponential introduced into $R$.

Using the Keyes form for $\psi, \psi=R / v-\delta, \delta=\beta e^{-\alpha / v}$, we can calculate $\delta$ for each isometric, using the value of $\psi$ from Table I, and these values of $\delta$ should be reproduced by an equation of the form $\log \delta=\log \beta-$ $\beta / 2.3 \mathrm{v}$. In Table II are given the deviations of the observed values from those calculated by the above equation.

For $\phi$, Keyes used $\phi=A /(v+l)^{2}$, and it was shown in the former paper on ether that this is equivalent to $\phi=\left(A / v^{2}\right) e^{-l / v}$, the latter form holding
${ }^{6}$ Using the "observed pressures" a considerable variation in $\psi$ and $\phi$ is possible when the isometric is curved, depending upon how the straight lines are drawn.
perhaps slightly better than the former. Table II gives a comparison of the observed $\phi$ 's from Table II with those calculated from the above equation. The check is not so satisfactory as in the case of the $\psi$ function.
A new $\phi$ function was chosen, namely, $\phi=\left(A / v^{2}\right) e^{-l / v^{2}}$ or $\log \phi v^{2}=$ $A-l / 2.3 v^{2}$.

## Table II

Comparison of Observed $\psi$ 's and $\phi$ 's with those Calculated from the Equation of State
The observed values of $\psi$ and $\phi$ are obtained from the linear equation given in Table $I$; the calculated values are from the following equation.

$$
\begin{aligned}
& \psi=R /(v-\delta)=1.10777 /(v-\delta) ; \delta=5.7630 e^{-5.3397 / v} ; \log _{10} \delta=0.76065-2.3190 / v \\
& \phi=\frac{5623.4}{v} e^{-1.4737 / v} ; \log _{10} \phi v^{2}=3.75000-0.64 / v \\
& \phi^{\prime}=\frac{5420.0}{v} e^{-13.797 / v^{2}} ; \log _{10} \phi v^{2}=3.73400-5.992 / v^{2}
\end{aligned}
$$

$R$ is in cc./atm. per ${ }^{\circ} \mathrm{C}$. per gram; $\psi$ in atm. per ${ }^{\circ} \mathrm{C}$.; $\phi$ in atm.; $v$ in cc. per gram.

| 0 | $\Delta \psi$$\times^{10-\mathbf{s}}$ | obs.-caled. | obs. - calcd. |
| :---: | :---: | :---: | :---: |
| 35 | -1 | -0.027 | -0.001 |
| 30 | 0 | -0.026 | -.008 |
| 25 | 0 | .006 | .005 |
| 20 | 2 | .035 | -.004 |
| 15 | -2 | -.025 | -.027 |
| 12.5 | -3 | -.261 | -.030 |
| 10 | 3 | -1.284 | .030 |
| 7.5 | 471 | -3.882 | +2.859 |

Table II gives a comparison of the observed and calculated $\phi$ values using this form of function. (In the table these values are designated by $\phi^{\prime}$.) It will be noticed that the values are reproduced satisfactorily over the same range that the $\psi$ values are reproduced, that is, down to and including 10 cc. per gram. Both functions fail to about the same extent at 7.5 cc . per gram.

Table III
Comparison of Observed Pressures with Those Calculated by the Equation of State
The first line gives the observed pressures; the second those calculated from the equation of state given; and the third the observed minus the calculated pressures.

| Vol., | ${ }^{\circ} \mathrm{T}$ Cmp. ${ }^{\text {Pro }}$ | 175 | 200 | 225 | 250 | 275 | 300 | 325 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 35 | 11.190 | 12.112 | 13.049 | 13.957 | 14.890 | 15.796 | 16.732 | 17.665 |
|  | 11.194 | 12.119 | 13.044 | 13.967 | 14.891 | 15.814 | 16.737 | 17.659 |
|  | - 0.004 | - 0.007 | 0.005 | - 0.010 | - 0.001 | - 0.018 | - 0.005 | 0.006 |
| 30 | 12.667 | 13.756 | 14.847 | 15.966 | 17.076 | 18.165 | 19.276 | 20.394 |
|  | 12.648 | 13.753 | 14.858 | 15.961 | 17.064 | 18.166 | 19.267 | 20.369 |
|  | 0.019 | 0.003 | - 0.011 | 0.005 | 0.012 | $-0.001$ | 0.009 | 0.025 |

Table III (Concluded)


In Table III is given a comparison of the original measured pressures with those calculated from the complete equation.

$$
\begin{array}{rlrl} 
& p=\frac{1.10777 T}{v-\delta}(1-\gamma)-\phi \\
\gamma & =\frac{0.00145}{v} e^{1596 / T} & \log _{10} v \gamma=\frac{693}{T}-2.83900 \\
\delta & =5.7630 e^{-5.3397 / T} & \log _{10} \delta=0.76065-2.319 / v \\
\phi & =\frac{5420}{v^{2}} e^{-13.797 / v^{2}} & \log _{10} v^{2} \phi=3.73400-5.992 / v^{2}
\end{array}
$$

This equation reproduces the measured pressures over the entire range above 10 cc . per gram. In only three cases are the deviations greater than 0.02 atmosphere and no deviation as great as 0.03 atmosphere occurs. This can be compared with the fit of the equation given in the earlier article in which the deviations were about 0.05 atmosphere at 15 cc . per gram and above, 0.3 atmosphere at 12.5 , and 1.6 atmospheres at 10 cc . per gram. Part of the betterment is due to the introduction of the new function of $t$ and $v$, but the greater part of the discrepancy is removed by the use of a new $\phi$ function, as can be seen by a comparison of Tables I and II.

Below 10 cc . per gram, different volume functions for $\phi$ and $\psi$ (or $\delta$ ) must be used. Series expansion of $\phi$ and $\psi$ in appropriate powers of $1 / v$ is probably the best method, at present, of representing the data in the region of high densities.

## Summary

The isometrics of gaseous ethyl ether are sensibly straight for large specific volumes, but show increasing curvature as the specific volume decreases.

If the curvature is supposed due to an aggregation of the molecules of the fluid, and the effect of this association is taken account of only in $R$, we obtain an equation of the following form for gaseous ethyl ether, when the fraction of molecules aggregated is small: $p=R T / v-. \delta$ $(1-\gamma)-\phi$, where $\delta=\beta e^{-\alpha / v}, \phi=\left(A / v^{2}\right) e^{-l / v^{2}}$, and $\gamma=(a / v) e^{b / T}$, Rearranging, this equation gives $p_{\text {corr. }}=p+[R T /(v-\delta)] \gamma=[R T /$ ( $v-\delta)]-\phi . \quad P_{\text {corr. }}$ should now vary linearly with the temperature along an isometric. For gaseous ethyl ether this is the case down to 5 cc . per gram. The above equation reproduced all the data down to 10 cc . per gram, no single measurement deviating as much as 0.03 atmosphere from the calculated pressure.

A new form for $\phi$, namely, $\left(A / v^{2}\right) e^{-l / v^{2}}$, has been suggested, and in the case of gaseous ethyl ether it represents the data better than forms previously used.

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[Contribution from the Research Laboratory of Physical Chemistry of the Massachusetts Institute of Technology, No. 192]

# AN EQUATION OF STATE FOR GASEOUS CARBON DIOXIDE 

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Equations of state have ordinarily been based on the perfect gas expression with the inclusion of appropriate correction terms to account for certain phenomena characteristic of actual gases, and these attempts ${ }^{2}$ have met with considerable success both theoretically and practically. On the other hand, there is a relation which approximates much more closely the behavior of all actual gases than does the perfect gas equation and which from the standpoint of thermodynamics is almost as general, namely, the linear relation between the pressure and the temperature of a gas when the volume is maintained constant. ${ }^{3}$ Departure from linearity becomes more marked at higher densities and lower temperatures, and association has been suggested ${ }^{2 b}{ }^{3 b}$ as the cause for the deviation from this relation which can be expressed mathematically as

$$
\begin{equation*}
P=\psi T-\phi \tag{1}
\end{equation*}
$$

[^2]
[^0]:    ${ }^{1}$ Beattie, This Journal, 46, 342 (1924).
    ${ }^{2}$ Keyes, Proc. Nat. Acad. Sci., 3, 323 (1917).

[^1]:    ${ }^{3}$ Boltzmann, "Vorlesungen über Gastheorie," Barth, Leipzig, vol. 2, chap. 6.
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